

ENT COOPERATION TRE

PCT

From the INTERNATIONAL BUREAU

NOTIFICATION OF THE RECORDING
OF A CHANGE(PCT Rule 92bis.1 and
Administrative Instructions, Section 422)

To:

DEAN, John, Paul
Withers & Rogers
Goldings House
2 Hays Lane
London SE1 2HW
ROYAUME-UNI

Date of mailing (day/month/year) 04 October 2001 (04.10.01)	IMPORTANT NOTIFICATION
Applicant's or agent's file reference	
International application No. PCT/GB00/02957	International filing date (day/month/year) 04 August 2000 (04.08.00)

1. The following indications appeared on record concerning:

☐ the applicant ☐ the inventor ☒ the agent ☐ the common representative

Name and Address BANNERMAN, D., G. Withers & Rogers Goldings House 2 Hays Lane London SE1 2HW United Kingdom	State of Nationality	State of Residence
	Telephone No.	
	Facsimile No.	
	Teleprinter No.	

2. The International Bureau hereby notifies the applicant that the following change has been recorded concerning:

☒ the person ☐ the name ☐ the address ☐ the nationality ☐ the residence

Name and Address DEAN, John, Paul Withers & Rogers Goldings House 2 Hays Lane London SE1 2HW United Kingdom	State of Nationality	State of Residence
	Telephone No.	
	Facsimile No.	
	Teleprinter No.	

3. Further observations, if necessary:

4. A copy of this notification has been sent to:

<input checked="" type="checkbox"/> the receiving Office	<input type="checkbox"/> the designated Offices concerned
<input type="checkbox"/> the International Searching Authority	<input checked="" type="checkbox"/> the elected Offices concerned
<input checked="" type="checkbox"/> the International Preliminary Examining Authority	<input type="checkbox"/> other:

The International Bureau of WIPO 34, chemin des Colombettes 1211 Geneva 20, Switzerland Facsimile No.: (41-22) 740.14.35	Authorized officer R. Raissi Telephone No.: (41-22) 338.83.38
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. ENT COOPERATION TP

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NOTIFICATION OF ELECTION

(PCT Rule 61.2)

From the INTERNATIONAL BUREAU

To:

Commissioner
 US Department of Commerce
 United States Patent and Trademark
 Office, PCT
 2011 South Clark Place Room
 CP2/5C24
 Arlington, VA 22202
 ETATS-UNIS D'AMERIQUE
 in its capacity as elected Office

Date of mailing (day/month/year) 10 April 2001 (10.04.01)	
International application No. PCT/GB00/02957	Applicant's or agent's file reference NPS/P71275WO
International filing date (day/month/year) 04 August 2000 (04.08.00)	Priority date (day/month/year) 05 August 1999 (05.08.99)
Applicant WILDE, Peter, Frederick	

1. The designated Office is hereby notified of its election made:

☒ in the demand filed with the International Preliminary Examining Authority on:
 05 March 2001 (05.03.01)

☐ in a notice effecting later election filed with the International Bureau on:

2. The election ☒ was
☐ was not

made before the expiration of 19 months from the priority date or, where Rule 32 applies, within the time limit under Rule 32.2(b).

The International Bureau of WIPO 34, chemin des Colombettes 1211 Geneva 20, Switzerland Facsimile No.: (41-22) 740.14.35	Authorized officer Juan Cruz Telephone No.: (41-22) 338.83.38
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PCT

INTERNATIONAL SEARCH REPORT

(PCT Article 18 and Rules 43 and 44)

Applicant's or agent's file reference NPS/P71275W0	FOR FURTHER ACTION see Notification of Transmittal of International Search Report (Form PCT/ISA/220) as well as, where applicable, item 5 below.	
International application No. PCT/GB 00/ 02957	International filing date (day/month/year) 04/08/2000	(Earliest) Priority Date (day/month/year) 05/08/1999
Applicant NATUROL LIMITED		

This International Search Report has been prepared by this International Searching Authority and is transmitted to the applicant according to Article 18. A copy is being transmitted to the International Bureau.

This International Search Report consists of a total of 3 sheets.

☒ It is also accompanied by a copy of each prior art document cited in this report.

1. Basis of the report

a. With regard to the **language**, the international search was carried out on the basis of the international application in the language in which it was filed, unless otherwise indicated under this item.

☐ the international search was carried out on the basis of a translation of the international application furnished to this Authority (Rule 23.1(b)).

b. With regard to any **nucleotide and/or amino acid sequence** disclosed in the international application, the international search was carried out on the basis of the sequence listing :

☐ contained in the international application in written form.

☐ filed together with the international application in computer readable form.

☐ furnished subsequently to this Authority in written form.

☐ furnished subsequently to this Authority in computer readable form.

☐ the statement that the subsequently furnished written sequence listing does not go beyond the disclosure in the international application as filed has been furnished.

☐ the statement that the information recorded in computer readable form is identical to the written sequence listing has been furnished

2. ☐ **Certain claims were found unsearchable** (See Box I).

3. ☐ **Unity of invention is lacking** (see Box II).

4. With regard to the **title**,

☒ the text is approved as submitted by the applicant.

☐ the text has been established by this Authority to read as follows:

5. With regard to the **abstract**,

☒ the text is approved as submitted by the applicant.

☐ the text has been established, according to Rule 38.2(b), by this Authority as it appears in Box III. The applicant may, within one month from the date of mailing of this international search report, submit comments to this Authority.

6. The figure of the **drawings** to be published with the abstract is Figure No.

☐ as suggested by the applicant.

☒ because the applicant failed to suggest a figure.

☐ because this figure better characterizes the invention.

1
☐ None of the figures.

PATENT COOPERATION TREATY

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INTERNATIONAL PRELIMINARY EXAMINATION REPORT


(PCT Article 36 and Rule 70)

Applicant's or agent's file reference NPS/P71275WO	FOR FURTHER ACTION	See Notification of Transmittal of International Preliminary Examination Report (Form PCT/IPEA/416)
International application No. PCT/GB00/02957	International filing date (day/month/year) 04/08/2000	Priority date (day/month/year) 05/08/1999
International Patent Classification (IPC) or national classification and IPC B01D11/02		
Applicant NATUROL LIMITED et al.		

1. This international preliminary examination report has been prepared by this International Preliminary Examining Authority and is transmitted to the applicant according to Article 36.
2. This REPORT consists of a total of 9 sheets, including this cover sheet.
- ☒ This report is also accompanied by ANNEXES, i.e. sheets of the description, claims and/or drawings which have been amended and are the basis for this report and/or sheets containing rectifications made before this Authority (see Rule 70.16 and Section 607 of the Administrative Instructions under the PCT).
- These annexes consist of a total of 7 sheets.

3. This report contains indications relating to the following items:

- I ☒ Basis of the report
- II ☐ Priority
- III ☐ Non-establishment of opinion with regard to novelty, inventive step and industrial applicability
- IV ☐ Lack of unity of invention
- V ☒ Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement
- VI ☐ Certain documents cited
- VII ☐ Certain defects in the international application
- VIII ☐ Certain observations on the international application

Date of submission of the demand 05/03/2001	Date of completion of this report 20.11.2001
Name and mailing address of the international preliminary examining authority:  European Patent Office D-80298 Munich Tel. +49 89 2399 - 0 Tx: 523656 epmu d Fax: +49 89 2399 - 4465	Authorized officer Edmueller, P Telephone No. +49 89 2399 2133



INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No. PCT/GB00/02957

I. Basis of the report

1. With regard to the **elements** of the international application (*Replacement sheets which have been furnished to the receiving Office in response to an invitation under Article 14 are referred to in this report as "originally filed" and are not annexed to this report since they do not contain amendments (Rules 70.16 and 70.17)*):
- Description, pages:**

1-21,23-26	as originally filed			
22	as received on	07/11/2001	with letter of	05/11/2001

Claims, No.:

1-38	as received on	07/11/2001	with letter of	05/11/2001
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Drawings, sheets:

1/1	as originally filed
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2. With regard to the **language**, all the elements marked above were available or furnished to this Authority in the language in which the international application was filed, unless otherwise indicated under this item.

These elements were available or furnished to this Authority in the following language: , which is:

- ☐ the language of a translation furnished for the purposes of the international search (under Rule 23.1(b)).
- ☐ the language of publication of the international application (under Rule 48.3(b)).
- ☐ the language of a translation furnished for the purposes of international preliminary examination (under Rule 55.2 and/or 55.3).

3. With regard to any **nucleotide and/or amino acid sequence** disclosed in the international application, the international preliminary examination was carried out on the basis of the sequence listing:

- ☐ contained in the international application in written form.
- ☐ filed together with the international application in computer readable form.
- ☐ furnished subsequently to this Authority in written form.
- ☐ furnished subsequently to this Authority in computer readable form.
- ☐ The statement that the subsequently furnished written sequence listing does not go beyond the disclosure in the international application as filed has been furnished.
- ☐ The statement that the information recorded in computer readable form is identical to the written sequence listing has been furnished.

4. The amendments have resulted in the cancellation of:

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International application No. PCT/GB00/02957

- ☐ the description, pages:
☐ the claims, Nos.:
☐ the drawings, sheets:

5. ☒ This report has been established as if (some of) the amendments had not been made, since they have been considered to go beyond the disclosure as filed (Rule 70.2(c)):

(Any replacement sheet containing such amendments must be referred to under item 1 and annexed to this report.)

see separate sheet

6. Additional observations, if necessary:

V. Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement

1. Statement

Novelty (N)	Yes:	Claims	1-5,8-12,22-24,27-28,31,34
	No:	Claims	15-21,37-38
Inventive step (IS)	Yes:	Claims	1-5,8-12,22-24,27-28,31,34
	No:	Claims	15-21,37-38
Industrial applicability (IA)	Yes:	Claims	1-5,8-12,15-24,27-28,31,34,37-38
	No:	Claims	

2. Citations and explanations

see separate sheet

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International application No. PCT/GB00/02957

Concerning section I, point 5.:

Newly added dependent claims 6,7, 13,14, 25,26, 29,30, 32,33 and 35,36 are considered to introduce subject-matter which extends beyond the content of the application as filed, contrary to Article 34(2)(b) PCT.

There appears to be no basis in the originally filed documents for the distinct process steps of (first) contacting the substrate with a solvent comprising iodotrifluoromethane to form a solution of the oil in the solvent followed by the separate step of adding one or more further solvents to the oil solution.

Therefore, dependent claims 6-7,13-14,25-26,29-30,32-33 and 35-36 have not been taken into account in this Report (Rule 70.2(c) PCT).

Concerning section V:

- 1.) The subject-matter of method claim 1 appears to be new in view of the disclosure of each of the documents cited in the International Search Report as none of these documents discloses the use of iodotrifluoromethane for extracting oil from an oil bearing substrate.

Therefore, it appears that claim 1 meets the requirements of Article 33(2) PCT.

- 2.) As closest state of the art in regard to the subject-matter of claim 1, the disclosure of document EP-A-0 616 821 = (D1) is taken.

(D1) discloses a method of extracting oil from an oil-bearing substrate comprising the steps of contacting the substrate with a non-chlorinated fluorinated hydrocarbon solvent (ie. 1,1,1,2-tetrafluoroethane), separating the solution from the substrate and removing the solvent from the solution to provide the desired oil (see examples 1 to 3).

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Claim 1 is distinguished from the disclosure of (D1) in that the substrate is contacted with a solvent comprising iodotrifluoromethane.

The objective technical problem to be solved with the distinguishing feature can be defined as being the provision of a method of extracting oil from an oil-bearing substrate in which method a solvent with higher solvating power is used.

None of the documents cited in the International Search Report gives any hint (alone or in combination) for solving the specified objective technical problem with the distinguishing feature.

Therefore, it appears that claim 1 meets the requirements of Article 33(3) PCT.

- 3.) Dependent claims 2 to 5 are preferred embodiments of the subject-matter of claim 1 and therefore also fulfil the requirements of Article 33 PCT.
- 4.) Concerning independent formulated claim 8 basically same argumentation applies as given in regard to claim 1 as claim 8 contains all the features of claim 1 (formal dependance on claim 1).

Therefore, it appears that claim 8 also meets the requirements of Article 33(2)(3) PCT.

- 5.) Dependent claims 9 to 12 are preferred embodiments of the subject-matter of claim 8 and therefore also meet the requirements of Article 33 PCT.
- 6.) Apparatus claim 15 lacks novelty in regard to the disclosure of document WO-A-00 43 471 = (D2) which represents a state of the art in accordance with Rule 64.1(a)(b) PCT for the reasons set out below:
 - a) (D2) discloses an apparatus suitable for the extraction of oil from an oil bearing substrate, the apparatus is specified by the identical apparatus features (= structural features) as the apparatus according to claim 15 (compare the apparatus according to figure 1 of (D2) with the apparatus according to figure 1 of the application in suit).

It has to be clearly said that any solvent and optionally any co-solvent does not structurally specify the claimed apparatus. In other words, iodotrifluoromethane solvent contained in the first vessel is not an apparatus feature and has to be completely disregarded.

- b) Because document (D2) relates to the same applicant as the application in suit and is novelty destroying to the subject-matter of apparatus claim 15 (and dependent apparatus claims 16 to 21), apparatus claim 15 and dependent claims 16 to 21 cannot enjoy the priority right of GB 991 8436 dated 05.08.1999 but rather the filing date of the present application (04.08.2000). In other words, the claimed priority GB 9918436 dated 05.08.1999 is not the first priority for the subject-matter of apparatus claims 15 to 21 of the application in suit as such subject-matter is already disclosed in document (D2) relating to the same Applicant {see requirements of Article 8(2)(a) PCT in combination with Article 4 of the Paris Convention for the Protection of Industrial Property}.
- 7.) Apparatus claim 15 also lacks novelty in regard to the disclosures of each of the documents US-A-43 31 695 = (D3) and GB-A-20 72 189 = (D4).

Each of the documents (D3) or (D4) discloses an apparatus which is suitable for the extraction of oil from an oil bearing substrate, the apparatus comprises first (1) and second (5,2) vessels, connecting means providing fluid communication between the vessels, at least one closable valve (8) operable to prevent fluid communication between the vessels, the first vessel being suitable to receive an oil bearing substrate and includes means (2) suitable for retaining an oil bearing substrate (see (D3), figure 1 in combination with column 3, line 51 to column 4, line 40; (D4), figure 1 in combination with page 2, lines 74 to 115).

It is repeated that iodotrifluoromethane solvent is not a structural part of the apparatus according to claim 15 (see paragraph 6a) above).

Therefore, it appears that apparatus claim 15 does not meet the requirements of Article 33(2)(3) PCT.

- 8.) Dependent apparatus claims 16 to 21 lack novelty in regard to the disclosure of document (D2) {see figure 1 in combination with page 14, line 15 to page 17, line

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6 and claims 9 to 14}.

Furthermore, it is referred to the statements under paragraphs 6a) and 6b) above.

Additionally, the features of dependent claims 20 and 21 are known from each of the documents (D3) and (D4) {see (D3), figure 1, reference numerals (3), (7) and column 3, lines 51 to 54; (D4), figure 1, reference numerals (6), (8) and page 2, lines 74-92}.

- 9.) Concerning independent formulated method claim 22 basically same argumentation applies as given in regard to claim 1 as claim 22 contains all the features of claim 1 (formal dependance on claim 1).

Therefore, it appears that claim 22 also meets the requirements of Article 33(2)(3) PCT.

- 10.) Dependent claims 23 to 24 represent preferred embodiments of the subject-matter of claim 22 and therefore also meet the requirements of Article 33 PCT.

- 11.) Regarding independent formulated method claim 27 basically same argumentation applies as given in regard to claim 1.

Therefore, it appears that method claim 27 also meets the requirements of Article 33(2)(3) PCT.

- 12.) Dependent claim 28 represents a preferred embodiment of the subject-matter of claim 27 and therefore also meets the requirements of Article 33 PCT.

- 13.) In regard to use claim 31 basically same argumentation applies as given in regard to the subject-matter of method claim 1.

Therefore, it appears that use claim 31 meets the requirements of Article 33(2)(3) PCT.

- 14.) In regard to independent formulated use claim 34 which claim is formally dependent on claim 31 basically same argumentation applies as given in regard to

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use claim 31.

Therefore, it appears that claim 34 meets the requirements of Article 33(2)(3) PCT.

- 15.) Product-by-process claim 37 which is directed to any oil, lacks novelty in regard to the disclosure of each of the documents (D1) to (D4) and in addition in regard to the disclosure of document WO-A-95 26 794 = (D5).

The obtained product according to each of the documents (D1) to (D5) is an oil (see (D1), examples 1-3, table 1, page 7, lines 13-15; (D2), claim 1, page 6, line 28 to page 7, line 11, example 1 on page 20 to page 22, line 3; (D3), examples 1-6; (D4), examples 1-2; (D5), claim 37, examples 1-10).

Concerning document (D2), attention is drawn to the fact that, similarly to the apparatus claims 15 to 21 of the application in suit, product-by-process claim 37 only enjoys the filing date (04.08.2000) as relevant date.

It has to be clearly said that a claim defining a product in terms of a process is to be construed as a claim to the product as such (in the present case any oil) and that a product is not rendered novel merely by the fact that it is produced by means of a new process.

Furthermore, attention has to be drawn to the fact that a spectrum of impurities contained in the claimed oil or the degree of impurities contained in the oil cannot render such product new as the impurities are not part of the claimed oil.

Therefore, it appears that product claim 37 does not meet the requirements of Article 33(2)(3) PCT.

- 16.) Product-by-process claim 38 which is directed to any vegetable oil suitable for use in foodstuffs lacks novelty in regard to the disclosure of each of the documents (D1), (D2), (D3) and (D5) {see (D1), page 2, lines 1-13, page 7, lines 13-15, examples 1-3, table 1; (D2), page 1, lines 3 to 14, page 6, lines 1 to 5, page 6, line 28 to page 7, line 11, example 1 on page 20 to page 22, line 3; (D3), column 1, line 57 to column 2, line 45, examples 1-6; (D5), page 1, third paragraph to page 2, line 26, page 3, first paragraph, examples 1-6}.

Regarding product-by-process claims and the relevant date of the subject-matter

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of claim 38 it is referred to paragraph 15.) above.

It is repeated that impurities contained in the claimed vegetable oil or the degree of impurities contained in the vegetable oil cannot render such product new as the impurities are not part of the claimed vegetable oil provided that the vegetable oil is suitable for use in foodstuff.

Therefore, it appears that product claim 38 does not meet the requirements of Article 33(2)(3) PCT.

- 17.) The industrial applicability of the claimed subject-matter is evident (Article 33(4) PCT).

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GB 00/02957

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 B01D11/02 B01D11/04 C11B1/10 C11B9/02 C10G1/04

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B01D C11B C10G

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data, PAJ

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
P, X	WO 00 43471 A (WILDE PETER FREDERICK ; NATUROL LIMITED (GB)) 27 July 2000 (2000-07-27) cited in the application page 7, line 13 - page 8, line 25 page 10, line 19 - line 30 page 13, line 5 - page 14, line 7; examples 1,2	11-17, 25, 26
X	US 4 331 695 A (ZOSEL KURT) 25 May 1982 (1982-05-25)	11-14, 16, 17, 25, 26
A	column 3, line 49 - column 4, line 40; figure 1; examples 1-7	1-10, 18-24
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☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

* Special categories of cited documents:

- *A* document defining the general state of the art which is not considered to be of particular relevance
- *E* earlier document but published on or after the international filing date
- *L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- *O* document referring to an oral disclosure, use, exhibition or other means
- *P* document published prior to the international filing date but later than the priority date claimed

- *T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- *X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- *Y* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
- *&* document member of the same patent family

Date of the actual completion of the international search

8 December 2000

Date of mailing of the international search report

14/12/2000

Name and mailing address of the ISA

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Authorized officer

Edmuller, P

INTERNATIONAL SEARCH REPORT

International Application No.

GB 00/02957

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X A	GB 2 072 189 A (KALI CHEMIE PHARMA GMBH) 30 September 1981 (1981-09-30) page 2, line 74 - line 115; figure 1; examples 1,2 ----	11-14, 16,17, 25,26 1-10, 18-24
X	WO 95 26794 A (ICI PLC ;POWELL RICHARD LLEWELLYN (GB); NAOOKES TIMOTHY JAMES (GB);) 12 October 1995 (1995-10-12) page 2, line 9 - line 26; claim 37; examples 1-10 ----	25,26
X	EP 0 616 821 A (ADVANCED PHYTONICS LTD) 28 September 1994 (1994-09-28) cited in the application examples 1-3; table 1 -----	25,26

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

GB 00/02957

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
WO 0043471	A	27-07-2000	AU 3062800 A GB 2345915 A	07-08-2000 26-07-2000
US 4331695	A	25-05-1982	AT 331374 B AR 196843 A AT 1099972 A BE 809028 A CA 1015373 A CH 581183 A DE 2363418 A DK 148691 B ES 421693 A FR 2211528 A GB 1446638 A IE 38654 B IT 1009074 B JP 55016200 B JP 49099302 A LU 69062 A NL 7317592 A, B, NO 141168 B SE 392907 B	25-08-1976 19-02-1974 15-11-1975 21-06-1974 09-08-1977 29-10-1976 11-07-1974 02-09-1985 01-05-1976 19-07-1974 18-08-1976 10-05-1978 10-12-1976 30-04-1980 19-09-1974 22-02-1974 25-06-1974 15-10-1979 25-04-1977
GB 2072189	A	30-09-1981	DE 3011185 A AR 222130 A AT 380479 B AT 132781 A AU 537973 B AU 6767381 A BE 887863 A CA 1153776 A CH 648765 A DD 157560 A DK 126381 A ES 499169 D ES 8201589 A FI 810799 A, B, FR 2478643 A GR 74833 A HU 188003 B IE 50893 B IL 62025 A IT 1135364 B JP 56145295 A NL 8100382 A NO 810957 A, B, NZ 196304 A PH 17788 A PT 72478 A, B SE 456997 B SE 8101622 A SU 984412 A US 4367178 A ZA 8100446 A	01-10-1981 15-04-1981 26-05-1986 15-10-1985 19-07-1984 01-10-1981 01-07-1981 13-09-1983 15-04-1985 17-11-1982 23-09-1981 16-12-1981 16-03-1982 23-09-1981 25-09-1981 12-07-1984 28-03-1986 06-08-1986 31-05-1984 20-08-1986 11-11-1981 16-10-1981 23-09-1981 07-12-1982 13-12-1984 01-03-1981 21-11-1988 23-09-1981 23-12-1982 04-01-1983 24-02-1982
WO 9526794	A	12-10-1995	AU 678104 B AU 1897095 A BR 9507212 A	15-05-1997 23-10-1995 09-09-1997

INTERNATIONAL SEARCH REPORT

information on patent family members

International Application No

GB 00/02957

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
WO 9526794 A		CA 2185422 A	12-10-1995
		CN 1147208 A	09-04-1997
		EP 0752903 A	15-01-1997
		JP 9510913 T	04-11-1997
		NZ 281989 A	27-05-1998
EP 0616821 A	28-09-1994	GB 2276392 A	28-09-1994
		CA 2115599 A	23-08-1994
		EP 1055439 A	29-11-2000
		IL 108652 A	15-07-1998
		US 5512285 A	30-04-1996

INTERNATIONAL SEARCH REPORT

International Application No

GB 00/02957

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 B01D11/02 B01D11/04 C11B1/10 C11B9/02 C10G1/04

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B01D C11B C10G

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data, PAJ

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category °	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
P,X	WO 00 43471 A (WILDE PETER FREDERICK ;NATUROL LIMITED (GB)) 27 July 2000 (2000-07-27) cited in the application page 7, line 13 -page 8, line 25 page 10, line 19 - line 30 page 13, line 5 -page 14, line 7; examples 1,2	11-17, 25,26
X	US 4 331 695 A (ZOSEL KURT) 25 May 1982 (1982-05-25)	11-14, 16,17, 25,26
A	column 3, line 49 -column 4, line 40; figure 1; examples 1-7 ----- -/--	1-10, 18-24

☒ Further documents are listed in the continuation of box C.☒ Patent family members are listed in annex.

° Special categories of cited documents:

A document defining the general state of the art which is not considered to be of particular relevance

E earlier document but published on or after the international filing date

L document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

O document referring to an oral disclosure, use, exhibition or other means

P document published prior to the international filing date but later than the priority date claimed

T later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

X document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

Y document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

Z document member of the same patent family

Date of the actual completion of the international search

8 December 2000

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INTERNATIONAL SEARCH REPORT

International Application No

GB 00/02957

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category °	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X A	GB 2 072 189 A (KALI CHEMIE PHARMA GMBH) 30 September 1981 (1981-09-30) page 2, line 74 - line 115; figure 1; examples 1,2 ---	11-14, 16,17, 25,26 1-10, 18-24
X	WO 95 26794 A (ICI PLC ;POWELL RICHARD LLEWELLYN (GB); NAOOKES TIMOTHY JAMES (GB);) 12 October 1995 (1995-10-12) page 2, line 9 - line 26; claim 37; examples 1-10 ---	25,26
X	EP 0 616 821 A (ADVANCED PHYTONICS LTD) 28 September 1994 (1994-09-28) cited in the application examples 1-3; table 1 -----	25,26

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

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INTERNATIONAL SEARCH REPORT

International Application No.

PCT/GB 00/00125

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 C11B1/10 C11B9/02 C10G1/04

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 C11B C10G

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 95 26794 A (ICI PLC ;POWELL RICHARD LLEWELLYN (GB); NAKES TIMOTHY JAMES (GB);) 12 October 1995 (1995-10-12) page 2, paragraph 2 page 3, paragraph 1 page 4, paragraph 6 -page 5, paragraph 3 examples 1,10	1-8
X	EP 0 616 821 A (ADVANCED PHYTONICS LTD) 28 September 1994 (1994-09-28) page 3, line 40-42 page 4, line 18-23 page 4, line 43 page 7, line 36-40 table 1	1-3,6-8
A	Examples	9-16

☒ Further documents are listed in the continuation of box C.☒ Patent family members are listed in annex.

* Special categories of cited documents :

"A" document defining the general state of the art which is not considered to be of particular relevance

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"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

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"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.

"Z" document member of the same patent family

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thermostat. The thermostat can be set to activate the immersion heater when the water temperature falls to for example 10°C and to switch off the heater whenever the temperature of the water exceeds for example 12°C. In this manner, the evaporator may be operated at about 10°C and the vapour pressure is 1 to 3 bar at the
5 compressor inlet.

The pressure contained the evaporator throughout this process is in the region of 30 psi. Once all the solution has passed from the extractor to the evaporator, and all the solvent from both the extractor and the evaporator has been evaporated, the vapour
10 pressure inside the evaporator begins to fall.

When this pressure had fallen to just above 0 psig an outlet on the bottom of the evaporator is opened so the oil solute (the extract) can run into a suitable receptacle. Weighing of the receptacle before and after the introduction of the oil reveals the
15 yield of fragrant oil.

Following removal of the oil, the compressor can be allowed to continue to suck residual solvent vapour from the extractor and from the substrate within it. By the time the pressure within the extractor has fallen to 100mbar over 99.9% of the
20 iodotrifluoromethane solvent will have been returned to the original reservoir.

To improve the recovery of solvent the extractor and the extracted substrate can be heated.

25 The present invention will now be illustrated by means of the following examples.

Example 1

At an ambient temperature of 20 degrees Celsius, 140 grams of peanut oil were
30 introduced into a PET bottle of capacity 2500 ml and designed to withstand 10 BarG. The bottle was fitted with an aerosol valve. This oil was dissolved in 780 grams of

CLAIMS

1. A method of extracting oil from an oil-bearing substrate comprising:
 - (a) contacting the substrate with a solvent comprising and, optionally, one or more co-solvents to form a solution of the oil in the solvent;
 - (b) separating the solution from the substrate; and
 - (c) removing the solvent from the solution to provide the desired oil.
2. A method as claimed in claim 1 further comprising contacting the solvent with the substrate in a first vessel and separating the resulting solution from the substrate by transferring the solution to a second vessel while retaining the extracted substrate in the first vessel.
3. A method as claimed in claim 2 wherein the first and second vessels are each sealable and each include an openable and closable valve, the method further comprising the steps of:
 - (i) connecting the vessels together to provide a flow path between the vessels via said valves; and
 - (ii) causing the solution to flow from the first vessel to the second vessel.
4. A method as claimed in claim 2 or 3 further comprising the step of applying heat to heat the solvent in the first vessel.
5. A method as claimed in any of claims 2 to 4 further comprising the step of cooling the solution in the second vessel.
6. A method of extracting oil from an oil-bearing substrate comprising:
 - (a) providing an apparatus comprising first and second sealable vessels, the first vessel including means for retaining said substrate in the vessel, each vessel having an inlet and an outlet and being so connected as to provide a fluid flow circuit only in the direction from the outlet of the first vessel to the

inlet of the second vessel and from the outlet of the second vessel to the inlet of the first vessel;

(ii) charging the oil bearing substrate into the first vessel;

5 (iii) charging the apparatus with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents so that the solvent contacts the substrate and forms a solution of the oil in the solvent;

(iv) causing said solution to flow in said fluid flow circuit from the first vessel to the second vessel; and

10 (v) separating the solvent from the oil in the second vessel and recovering the oil.

7. A method as claimed in claim 6 further comprising the step of applying heat to the solvent in the first vessel, or adjacent the inlet of the first vessel.

15 8. A method as claimed in claim 6 or 7 further comprising the step of cooling the contents of the second vessel.

9. A method as claimed in any of claims 6 to 8 further comprising recovering the separated solvent for use in further extractions.

20

10. A method as claimed in any preceding claim wherein the optional co-solvent is selected from HFC 134a and HFC 4310.

11. An apparatus for the extraction of oil from an oil bearing substrate comprising first and second vessels, connecting means providing fluid communication between the vessels, at least one closable valve operable to prevent fluid communication between the vessels, the first vessel being adapted to receive the oil bearing substrate and including means for retaining the substrate in the first vessel, and, a solvent provided in the first vessel comprising iodotrifluoromethane and, optionally at least one co-solvent.

25

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which solvent may be transferred between the first and second vessels via the or each closable valve.

- 5 12. An apparatus as claimed in claim 11 wherein each vessel comprises an inlet and an outlet, the outlet of the first vessel is connected by first connecting means to the inlet of the second vessel, the outlet of the second vessel is connected by second connecting means to the inlet of the first vessel, the first and second connecting means include at least one said closable valve, and each closable valve is a one-way valve permitting fluid flow in one direction only, the valves being arranged to provide a fluid flow circuit such that the solvent may flow around the circuit in one direction only.
- 10 13. An apparatus as claimed in claim 12 wherein one closable one-way valve is provided at each respective inlet and each respective outlet of the first and second vessels.
- 15 14. An apparatus as claimed in claim 12 or 13 including heating means for heating the solvent in the first vessel or adjacent to the inlet of the first vessel.
- 20 15. An apparatus as claimed in any of claims 12 to 14 including cooling means for cooling the contents of the second vessel.
- 25 16. An apparatus as claimed in any of claims 11 to 15 further comprising a reservoir of solvent operatively connectable to the fluid flow circuit.
17. Apparatus as claimed in any of claims 11 to 16 further comprising means for withdrawing, from the second vessel or from the connecting means adjacent the second vessel, oil which has separated from the solvent.
- 30 18. A method of extracting oil from an oil bearing substrate comprising the steps of:

- (i) contacting the substrate with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents thereby to dissolve the oil in the solvent; and
- (ii) causing the oil to separate from the solvent to form immiscible liquid layers of oil and solvent.
- 5
19. A method as claimed in claim 18 wherein step (ii) involves cooling the solution of oil in the solvent.
- 10 20. A method as claimed in claim 18 or 19 wherein step (i) includes heating the solvent.
21. A method of extracting oil from an oil-bearing substrate comprising the steps of:
- 15 (i) contacting the substrate with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents, thereby to dissolve the oil in the solvent; and
- (ii) allowing the solvent to evaporate at ambient or sub-ambient temperatures.
- 20
22. A method as claimed in claim 21 further comprising recovering the evaporated solvent and compressing the solvent to re-liquify it.
23. Use of iodotrifluoromethane for the extraction of oil from an oil-bearing substrate.
- 25
24. Use of a solvent comprising iodotrifluoromethane and at least one co-solvent for the extraction of oil from an oil-bearing substrate.
- 30 25. An oil obtainable by, or when obtained by, the method of any of claims 1 to 10 or 18 to 22.

26. A vegetable oil for use in foodstuffs obtainable by, or when obtained by, the method of any of claims 1 to 10 or 18 to 22 and containing substantially no residue of solvent, especially iodotrifluoromethane.

5

PROCESS AND APPARATUS FOR PREPARING EXTRACTS AND OILS FROM PLANTS AND OTHER MATTER

The present invention relates to a method of extracting and concentrating oils from materials in which the oils are already dispersed. More particularly, the present invention is concerned with the extraction of fixed and mineral oils and/or volatile oils such as essential oils from materials using a process of solvent extraction which is performed under pressure.

10 The term "Fixed Oil" is usually used to describe oils of vegetable or animal origin which are not volatile oils. They routinely comprise natural mixtures of mono-, di and tri-glycerides, fatty acids, sterols (and their esters) and natural waxes.

"Mineral Oil" is a term usually used to describe petrochemical oils often derived from below ground level, which are normally mixtures of aliphatic and aromatic hydrocarbons of a very wide variety of chain length and molecular weight. These oils are often the sources of lubricating and fuel oils.

The term "Essential Oil" is usually used to describe those volatile oils of low molecular weight which incorporate the fragrance and flavour of components derived from plant materials.

In an earlier application (GB 2276392) we described the use of HFC 134A (1, 1, 1, 2 - tetrafluoroethane) as a solvent for the extraction of essential oils from natural sources.

However HFC 134a is in fact a very poor solvent for many compounds, particularly less volatile compounds. Thus, whilst HFC 134a is able to dissolve some essential oils thereby facilitating extraction of such oils from plant-based materials, this solvent is not able easily to dissolve compounds of lower volatility such as fixed oils. HFC 134a is therefore capable at ambient temperatures of extracting only very high

quality fragrant and aromatic essential oils i.e. delicate oils of high volatility and low molecular weight and it will not dissolve the fixed oils which are also frequently associated with these components in the natural raw material.

- 5 Because HFC 134a is a very poor solvent, large quantities of it must be used in order to obtain a commercially acceptable yield of the desirable component extracted from most raw materials.

10 In another unpublished application (GB 9905054.4) we describe a process in which HFC 134a is used to extract fixed and mineral oils from a substance. This process relies on the unexpected finding that raising the temperature only a few degrees Celsius results in a marked increase in the solubility of fixed and mineral oils in HFC 134a. The process is conducted in a sealed apparatus including a first vessel in which the substance is contacted with HFC 134a at an elevated temperature and a
15 second vessel in which the HFC 134a (now containing dissolved fixed or mineral oil) is cooled. The fixed or mineral oil is precipitated out of the solution and can easily be separated from the HFC 134a solvent which is then recycled to minimise losses and environmental impact.

20 In a variation of the process described in our unpublished application GB 9905054.4, the solvent may be a mixture of HFC 134a and a co-solvent in which the fixed or mineral oil to be extracted is relatively soluble. The dissolving properties of HFC 134a are significantly increased by the addition of a suitable co-solvent. Suitable co-solvents which can be added to HFC 134a may be liquids at room temperature or
25 liquefied gases and include hydrocarbons such as the alkanes, benzene and its esters, low boiling aliphatic esters such as acetates and butyrates, ketones such as acetone, methyl isobutyl ketone, methyl ethyl ketone, chlorinated, fluorinated and chlorofluorinated hydrocarbons such as dichloromethane and dichloro
30 difluoromethane, ethers and such as dimethyl ether and diethyl ether, dimethyl formamide, tetrahydrofuran, dimethyl sulphoxide, alcohols such as methyl alcohol, ethyl alcohol, n-propanol, iso-propanol, acids such as acetic acid, formic acid and

even acetic anhydride, nitriles such as acetonitrile (methyl cyanide), anhydrous liquefied ammonia and other liquefied gases such as sulphur dioxide, nitric oxide, nitrogen dioxide, nitrous oxide, liquefied hydrogen sulphide, carbon disulphide, nitromethane, and nitrobenzene could all be used in this process.

5

The most useful co-solvents have proved to be butane and dimethyl ether. Regrettably, though, many of the useful co-solvents which are mixed with HFC 134a re-confer the serious hazard of flammability on the mixtures and therefore raise safety issues. There may, depending on the choice of co-solvent, be other problems such as environmental issues.

10

Although it is neither a serious ozone depleter nor a VOC, unfortunately HFC 134a is a potent and powerful greenhouse gas. It has a global warming potential or greenhouse effect some 8 times as strong as carbon dioxide. HFC 134a is very chemically inert and persists in the environment for very long periods of time, during its decomposition. It has a $t_{1/2}$ life between 8.6 and 16.7 years.

15

Historically solvents such as hexane, petroleum fractions, benzene, methylene chloride (dichloromethane) have been widely used to extract oils from an enormous range of flavoursome oleo-resins, drug containing extracts and fragrant raw materials ("concretes"). These solvents are in common use even in the engineering, petroleum and mineral industries, where they are often used to de-grease raw materials containing or coated in oil and to clean metal parts, by the removal of oily lubricating preparations. Useful amounts of oils have even been extracted from mineral raw materials such as oil shales and tar sands with such solvents. Even soils contaminated with oily industrial waste may be remediated with such solvents.

20

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As they are all highly flammable, one disadvantage of conventional solvent systems such as hydrocarbon solvents, for example hexane and benzene and petroleum fractions, has always been the dangers of fire or explosion and incineration. These solvents also present further hazards to the operators of such processes because many

30

hydrocarbon and chlorinated solvents are harmful or toxic by inhalation and ingestion. They are frequently carcinogenic and all of the hydrocarbon solvents used in current practice are classed as VOCs (volatile organic compounds) which are said to have a positive photo-chemical ozone generating potential.

5

A further disadvantage of the most commonly used solvents, hexane and "petroleum ether", is that their boiling points (at atmospheric pressure) are in excess of 50 degrees Celsius. Hence, in order to remove such solvents from the solutions of the desired components, the desired component must either be exposed to high
10 temperatures or high vacuum. Both of these treatments detract from and are damaging and deleterious to the quality of the desired component or extract. Also, the evaporation of the solvent from the solution of the oil, and the solvent recovery by condensation is expensive on account of the energy costs.

15 The finished products from such processes are often intended for public consumption and the presence of toxic or harmful residues may present difficulties when seeking regulatory approval of the finished product.

These problems become even more serious when (as is increasingly the case)
20 statutory authorities are demanding that the solvent residue levels in oils sold for use in human food stuffs are required to meet increasingly stringent requirements such as solvent residue levels of only 50, 10 and even 1 part per million. Achieving such levels of solvent residue requires that the solution and extract be exposed to very high vacuum and/or very high temperatures. Such treatment can result in serious loss of
25 the precious volatile components from the extracts and serious thermal damage to the desirable component.

A strategy to overcome these problems has long been to employ hydrocarbon solvents such as butane and even propane (in liquid form under pressure). However,
30 these processes are even more dangerous, of course, as any leakage of the (usually

odourless) solvent vapours from the operating equipment, poses a greatly enhanced risk and chance of explosion and incineration.

5 The use of less flammable solvents such as chlorinated hydrocarbon solvents has gone some way to reducing these risks. For example, the use of methylene chloride (dichloromethane) to extract valuable components such as caffeine from coffee and tea has become common. Similarly, perchloroethylene has a long history of use in the dry cleaning industry to de-grease oily clothing.

10 However, many of the traditional chlorinated solvents present their own problems. Most of these materials are either harmful or toxic or may be damaging to the environment. Their vapours are believed to deplete the protective ozone in the stratosphere. Many of these chlorinated solvents are also greenhouse gases and may lead to global warming.

15

The process and apparatus we now describe in this specification are of great value in the extraction of high quality, desirable components such as oils, pigments, pharmacologically active ingredients and resins from a wide range of substrates comprising plant, animal and mineral matter, of both terrestrial and marine origin.

20 The same process and apparatus, when using the solvent systems according to an embodiment of the invention, are able to extract fixed and mineral oils.

The process comprises the contacting of the substrate (such as a bulk raw material) in which the desired component is already contained, with a solvent so as to allow the
25 desired component to dissolve in the solvent. It provides for the removal and separation of the substrate from the solution of the desired component in the solvent. It further provides for the removal of the solvent from the solution and its recovery for recycling and re-use, and for the harvesting of the solute from which the solvent has been removed. The solute - in such cases - comprises the desired component.

30

The extraction of desirable components from a substrate in many of the prior art processes must be carried out in sealed (pressure vessel) equipment. In any solvent extraction process it is normally highly desirable for economic and environmental reasons to collect as much of the used solvent from the solution formed (of the solvent and the desirable component) and from the spent and extracted bulk raw material. Nevertheless it is inevitable that some loss of solvent vapour into the atmosphere always occurs.

This consideration has lead us to search for a solvent which has more acceptable physiological and environmental characteristics and which is also an effective solvent capable of extracting fixed, mineral and essential oils.

The present invention thus aims to provide an economical process which is also able to provide the extracted oils in relatively high yield. It is also an aim to provide a quick extraction process which can be used commercially.

It is also an aim to provide a process which is easy to run and which does not require bulky or complicated apparatus. It is another aim to use a solvent which is not environmentally damaging and which does not have any significant photochemical ozone generating potential. Such a process aims to eliminate or reduce the losses of solvent during the extraction process. Indeed, it is a further aim to provide a process in which solvent losses are minimised so that there is substantially 100% solvent recovery.

It is also an aim to avoid the risk of fire or explosion by using a non-flammable solvent system, or at least a system having a significantly reduced risk of fire or explosion.

It is also an aim to minimise the content of any toxic solvent residues in the final product and preferably to achieve a product in which there are substantially no toxic solvent residues. It is an aim that the extracted oil be substantially free of traces of

solvent so that the extracted oil may easily satisfy any present or future regulatory requirements.

5 It is also intended to dispense with the need for the elimination of, or evaporation and condensation of, large quantities of solvents in order to obtain the final product from the solvent.

We have found that iodotrifluoromethane (ITFM) satisfies most or all of these requirements.

10

According to a first aspect of the invention there is provided a method of extracting oil from an oil-bearing substrate comprising:

- (a) contacting the substrate with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents to form a solution of the oil in the solvent;
- 15 (b) separating the solution from the substrate; and
- (c) removing the solvent from the solution to provide the desired oil.

In a first embodiment of this aspect of the invention the method comprises contacting the solvent with the substrate in a first vessel and separating the resulting solution
20 from the substrate by transferring the solution to a second vessel while retaining the extracted substrate in the first vessel.

Preferably the first and second vessels are each sealable and each include an openable and closable valve, the method further comprising the steps of:

- 25 (i) connecting the vessels together to provide a flow path between the vessels via said valves; and
- (ii) opening the valves of the vessels and causing the solution to flow from the first vessel to the second vessel.

In a particularly preferred embodiment, the method further comprises the step of applying heat to heat the solvent in the first vessel. This step facilitates the dissolution of the oil in the solvent.

- 5 In another particularly preferred embodiment, the method further comprises the step of cooling the solution in the second vessel. This cooling step can cause the oil to precipitate from the solvent, so that the oil and solvent can be separated.

According to a second aspect of the invention there is provided a method of
10 extracting oil from an oil-bearing substrate comprising:

- (i) providing an apparatus comprising first and second sealable vessels, the first vessel including means for retaining said substrate in the vessel, each vessel having an inlet and an outlet and being so connected as to provide a fluid flow circuit only in the direction from the outlet of the first vessel to the inlet of the second vessel and
15 from the outlet of the second vessel to the inlet of the first vessel;
- (ii) charging the oil-bearing substrate into the first vessel;
- (iii) charging the apparatus with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents so that the solvent contacts the substrate and forms a solution of the oil in the solvent;
- 20 (iv) causing said solution to flow in said fluid flow circuit from the first vessel to the second vessel; and
- (vi) separating the solvent from the oil in the second vessel and recovering the oil.

This aspect of the invention provides a continuous process for extracting oil from a
25 substrate.

In a particularly preferred embodiment of this aspect of the invention, the method further comprises the step of applying heat to the solvent in the first vessel, or adjacent the inlet of the first vessel. This heating step facilitates dissolution of the oil
30 in the solvent.

In another particularly preferred embodiment, the method further comprises the step of cooling the contents of the second vessel. This cooling step can cause the oil to precipitate from the solvent for subsequent separation and recovery.

- 5 Preferably the method of this aspect of the invention further comprises recovering the separated solvent for use in further extractions.

In particularly preferred embodiments of the first and second aspects of the invention, the optional co-solvent is selected from HFC 134a and HFC 4310.

10

Iodotrifluoromethane has the advantage that it has no global warming potential and is not a VOC. It is not flammable, indeed actually used as fire extinguisher. It does not deplete the ozone layer, is effectively non-toxic and represents virtually no biological hazard or environmental threat. It has a very low boiling point (- 22.5 degrees
15 Celsius at atmospheric pressure) and a modest vapour pressure of only 63.7 psi (4.3 Bar) at 25 degrees Celsius.

20

ITFM is an excellent extraction medium and solvent for many of the oils of commerce including triglycerides, fatty acids, sterols and their esters, natural waxes, hydrocarbons (both straight and branched chains and cyclic and poly-cyclic) with
molecular weights up to several hundreds. It also dissolves fragrance oils, pigments, flavour oils and many pharmaceutical components from natural plant and animal raw materials. For these uses in the process of the invention, it is not usually necessary to perform a heating step.

25

ITFM also presents no special problems in handling and recovery for recycling.

30

Although ITFM is currently a costly solvent, the financial penalty attendant on its use may be minimised using the process of the present invention since almost complete solvent recovery occurs. Furthermore, the solvent offers tremendous advantages to the environment.

Because it has a low boiling point, extraction of and recovery of desirable components can be carried out at room temperature or below, thus eliminating any chance of thermal degradation or damage to the extracts that often occurs when other solvents are used. Iodotrifluoromethane (ITFM) is pH neutral and does not hydrolyse appreciably in water at room temperature.

Should it be necessary to reduce the wide spectrum of solutes which dissolve in iodotrifluoromethane (ITFM) (i.e. to render it more selective), it can be mixed with one or more poor or non-solvents. Suitable poor solvents or non-solvents are for example, HFC 134a (1,1,1,2-tetrafluoroethane) or HFC 4310 (1,1,1,2,2,3,4,5,5,5-decafluoropentane). This may be done to impart selectivity to the extraction process in order to enhance the amount of a particular oil in a mixture of extracted oils. In this case, since the co-solvent (such as HFC 134a) only represents a part of the solvent mixture (rather than being the sole solvent) any problems which may be associated with the co-solvent itself are minimised.

A feature of the invention thus makes use of the property of mixtures of ITFM and one or more suitable co-solvents to dissolve to specified and finite limits of molecular weight or polarity. This confers a degree of selectivity on the solvent mixtures to extract components of specified molecular weight, such as volatile components of fragrance oils, whilst excluding from solution many of the materials which would then be considered to be undesirable contaminants, such as triglycerides, fatty acids and natural waxes. It is, however, important that the presence of the co-solvent still provides a solvent system which meets statutory or other requirements relating to toxicity or other health hazards.

A related feature of this invention also makes use of the observation that certain mixtures of ITFM with one or more suitable co-solvents do not dissolve fixed oils such as triglycerides, fatty acids, natural waxes, mineral oils and petroleum fractions etc at low temperatures. At elevated temperatures, such solvent mixtures do in fact

dissolve these materials. Hence it becomes a simple matter to dissolve such fixed and mineral oils and extract them from the substrate such as bulk raw material in which they occur by heating the solvent mixture in the presence of the substrate. Removal of the heated solution and cooling it causes the solutes to precipitate from solution in all cases. The solutes (being of lower specific gravity than the solvent) float to the top of the cooled solution and can be easily harvested. In this case, the method would involve the step of elevating the temperature and the step of cooling the separated solvent solution once it has been transferred to the second vessel so as to release any dissolved oil. At this point, either the released oil or the iodotrifluoromethane solvent can be removed from the second vessel to complete the separation.

The invention also relates to an apparatus for performing oil extraction.

According to a third aspect of the invention there is provided an apparatus for the extraction of oil from an oil-bearing substrate comprising first and second vessels, connecting means providing fluid communication between the vessels, at least one closable valve operable to prevent fluid communication between the vessels, the first vessel being adapted to receive the oil-bearing substrate and including means for retaining the substrate in the first vessel, and, a solvent provided in the first vessel comprising iodotrifluoromethane and, optionally at least one co-solvent, which solvent may be transferred between the first and second vessels via the or each closable valve.

In an especially preferred embodiment of this aspect of the invention, each vessel comprises an inlet and an outlet, the outlet of the first vessel is connected by first connecting means to the inlet of the second vessel, the outlet of the second vessel is connected by second connecting means to the inlet of the first vessel, the first and second connecting means include at least one said closable valve, and each closable valve is a one-way valve permitting fluid flow in one direction only, the valves being arranged to provide a fluid flow circuit such that the solvent may flow around the

circuit in one direction only. This embodiment allows a continuous extraction process to be carried out.

5 Preferably one closable one-way valve is provided at each respective inlet and each respective outlet of the first and second vessels. In this way, the first and second vessels can be isolated as required.

10 Preferably the apparatus includes heating means for heating the solvent in the first vessel or adjacent to the inlet of the first vessel and/or cooling means for cooling the contents of the second vessel.

15 In a desirable for the apparatus further comprises a reservoir of solvent operatively connectable to the fluid flow circuit. Preferably, the apparatus also includes means for withdrawing solvent from the fluid flow circuit. Desirably, the point for addition of solvent from the reservoir and/or the point for withdrawal of solvent is/are between the outlet of the second vessel and the inlet of the first vessel.

20 Preferably the apparatus further comprises means for withdrawing, from the second vessel or from the connecting means adjacent the second vessel, oil which has separated from the solvent.

In a further embodiment, the apparatus includes means for determining the pressure in the circuit and/or the temperatures of the first and second vessels.

25 In a further embodiment, the first and second vessels are transparent pressure vessels capable of withstanding pressures of not more than 25 bar.

A fourth aspect of the present invention provides a method of extracting oil from an oil-bearing substrate comprising the steps of :

30 (i) contacting the substrate with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents thereby to dissolve the oil in the solvent; and

(ii) causing the oil to separate from the solvent to form immiscible liquid layers of oil and solvent.

Preferably step (ii) involves cooling the solution of oil in the solvent.

5

Also preferably step (i) includes heating the solvent.

A fifth aspect of the invention provides a method of extracting oil from an oil-bearing substrate comprising the steps of:

- 10 (i) contacting the substrate with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents, thereby to dissolve the oil in the solvent; and
(ii) allowing the solvent to evaporate at ambient or sub-ambient temperatures.

15 In a preferred embodiment of this fifth aspect of the invention the method further comprises recovering the evaporated solvent and compressing the solvent to re-liquify it.

The present invention also contemplates the use of iodotrifluoromethane for the extraction of oil from an oil bearing substrate, and also the use of a solvent
20 comprising iodotrifluoromethane and at least one co-solvent for the extraction of oil from an oil-bearing substrate.

The present invention further includes an oil obtainable by, or when obtained by, the method of any of the first, second or fourth aspects of the invention.

25

The present invention also includes a vegetable oil for use in foodstuffs obtainable by or when obtained by, the method of any of the first, second or fourth aspects of the invention and containing substantially no residue of solvent, especially iodotrifluoromethane.

30

The appropriate co-solvent, and the iodotrifluoromethane:co-solvent ratio for a given substance are determined as follows.

5 An empty bottle together with a removable seal is weighed and the weight recorded (Weight A). This assembly should be designed to be able to withstand a pressure of say 10 BarG.

10 Into the bottle is placed a sample of the substance i.e. the oil-containing substrate (raw material) to be extracted, or a sample of the oil itself.

The bottle and seal is weighed again and the weight recorded (Weight B). The bottle is then closed and sealed. The difference between weight B and weight A is the weight of the substrate containing oil or the oil.

15 The iodotrifluoromethane alone is introduced into the bottle and the mixture shaken until the contents are homogenous and the solute is in complete solution. The bottle and contents are weighed again and the final weight of the bottle and contents are recorded (Weight C). The difference between Weight B and Weight C is the weight of the added iodotrifluoromethane.

20 Co-solvent in which the solute is only poorly soluble or in which it is insoluble is then progressively introduced into the bottle. At first no obvious change takes place, but as the quantity of co-solvent is increased, the contents of the bottle will be seen to turn from crystal clear to opalescent. The weight of the bottle and contents is again
25 recorded (Weight D). The difference between Weight D and Weight C is the quantity of co-solvent added.

30 In order to ensure that the precipitation of oil from the mixture has reached its optimum, the bottle may now be placed in a refrigerator, whereupon the contents will first become cloudy and soon a clear and distinct layer of oil will separate and float on the lower layer of clear solvent. The solvent at low temperature can then be

withdrawn and introduced to another bottle charged with more of the oil or the oil-containing substrate (raw material). This cold solvent will not dissolve the oil, but on warming, it will be seen to form a homogeneous solution (which will itself separate again into two layers on cooling).

5

This procedure will allow calculation of the composition of a solvent mixture. For example: The total weight of solvent used is $D - B$. The weight of iodotrifluoromethane is $C - B$ and the weight of co-solvent is $D - C$.

10 Hence the weight % composition of the solvent is:

$$\begin{array}{ll} \text{iodotrifluoromethane} & = (C - B / D - B) \times 100\% \\ \text{co-solvent} & = (D - C / D - B) \times 100\% \end{array}$$

15 The % concentration of solute in the solution
 $= (B - A / D - A) \times 100\%$

The invention will now be described with reference to Figure 1 which shows an apparatus suitable for continuous extraction of fixed and mineral oils according to one embodiment of the process of the present invention.

20 Two vessels (1) and (2) equipped with closable valves were coupled together via two sets of tubing (3, 4). Both vessels are capable of withstanding pressure typically up to 25bar. Below vessel (1), the tubing (3) was in the form of a coil (5) sitting in a bath of liquid (6) which could be heated and maintained at a pre-selected temperature. The coil of tubing (5) could, however, be heated by another means or vessel (1) could be heated directly.

25 Vessel (1) was equipped with internal filters (7) at both ends, whereas vessel (2) was
30 equipped with a filter (8) only at the lower end.

The second vessel (2) was surrounded by coils (9) containing a flow of cooling liquid and the outside of the coils was insulated. Other means of cooling vessel (2) could also be used, for example a stream of cooling gas or a cooling bath.

- 5 The circuit was furnished with an inlet (10) and outlet (11) valves for solvent. During operation of the equipment, the inlet valve was coupled to a solvent reservoir (12) which could be used to both fill the system with solvent and maintain the level of solvent during operation. Outlet valve (11) was provided to enable the system to be drained.

10

At the top of vessel (2), a valve (13) is fitted to facilitate the recovery of oil when this becomes necessary or desirable. A pressure gauge (16) may be provided in the circuit.

- 15 The same equipment can be used regardless of whether the solvent is iodotrifluoromethane alone or in combination with a co-solvent, and regardless of whether any heating or cooling is actually performed.

20 The operation of the equipment is for the purpose of illustration only described as follows in relation to a mixture of iodotrifluoromethane and a co-solvent to extract a fixed oil.

1. Vessel (1) (which has removable end caps) is charged with the substrate from which oil is to be extracted (usually in the form of a finely divided particulate solid).
- 25 The end caps and filters are then replaced. The vessel is then connected to the remainder of the equipment. Air is then removed from the sealed equipment at this stage.
2. The equipment (now fully sealed) is then fully charged with solvent from the bulk solvent storage tank (12) (which remains connected to the equipment throughout
- 30 the operation).

3. The heating bath (6) is then filled with water or oil and the heating means turned on if required.

4. If required, cold liquid or gas is circulated round the cooling coils (5) causing the temperature of the second vessel (2) (and its contents) to cool.

5

As the temperature of the liquid in the heating bath rises, so does the temperature of solvent in the tube below vessel (1). This, of course, causes hot solvent in vessel (1) to rise through the oil containing substrate of the vessel (1) due to natural convection. The substrate is restrained inside vessel (1) by the filters (7) disposed at the top and
10 bottom. The liquid displaced upwards is replaced by cold liquid falling through vessel (2) due to convection.

The entire liquid in the circuit thus becomes mobile and circulating. As hot liquid passes up through the substrate of vessel (1) oil is exacted from the substrate. As the
15 solution enters the top of vessel (2) it is cooled and its solute (the oil) precipitates out of solution.

Alternatively, in the absence of heating and the resulting convection currents which occur, the solvent may be pumped around the circuit.

20

Because the oil is lighter than the solvent, it floats to the top of vessel (2) and collects there as it is not able to pass out of the bottom of vessel (2).

When it is considered that sufficient oil has been extracted, all the valves are closed
25 except valve (14) (the inlet valve for vessel (2)) and valve (15) (the outlet valve for vessel (2)). Valve (13) is then opened to release the oil and the oil can be decanted into a bottle.

The system may be emptied after use by allowing solvent to drain out of valve (1)
30 into a suitable container for recycling and recovery by evaporation.

It will be immediately apparent to one versed in the art, that this process is capable of producing oil without any evaporative step. Since evaporation of the solvent is one of the major costs involved in more traditional methods of extraction, this constitutes a major improvement in the extraction of such oils and represents a significant cost saving.

Since iodotrifluoromethane is neither flammable, nor toxic, nor environmentally damaging and (in normal operation) is never released into the environment, the process of the present invention represents a significant improvement over current technologies.

In another embodiment of the process (not shown), the apparatus comprises two sealable vessels (which are preferably transparent and made of strengthened or reinforced glass) each being capable of withstanding a pressure of up to 20 bar or even 25 bar. Each vessel is equipped with a closable valve which acts as an inlet and an outlet valve. One vessel is also equipped with a removable filtering device, such as a wire gauze or wire wool to prevent the exit of raw material from the vessel at the same time as the solvent is withdrawn.

The two vessels are connected to each other via their inlet/outlet valves so as to form a sealed unit. Typically each vessel is 50mls to 2000mls capacity, and preferably 100mls to 500mls. Such an apparatus is easily assembled and handled. However, there are no particular limitations other than the usual practical limitations, on the upper size of such apparatus.

In this embodiment (not shown), it is possible to extract a fixed or mineral oil from a substance in an apparatus comprising two vessels which is not arranged in the form of a circuit. The substrate (raw material) is placed in a first vessel and the extraction medium (i.e. the solvent) is also introduced into the first vessel. The inlet/outlet valve of both vessels are then closed and the ensemble is warmed, typically to 40°-

60° (and preferably not more than 50°C), in an oven or using other suitable heating means. The apparatus may be agitated during heating or may contain agitation means such as a magnetic flea.

- 5 After an appropriate residence time at the elevated (holding) temperature, typically in the range 1 to 20 minutes and preferably in the range 3 to 8 minutes from the point of view of efficiency and cost effectiveness, the solution is transferred from the first vessel to the second vessel and the ensemble is cooled to room temperature or lower. Ideally, the ensemble is cooled to a temperature in the range -10° to 25°C and
10 preferably in the range 0° to 20°C. Cooling below -10°C is possible but increases the costs and complexity of the process.

Transfer of the solution is achieved via the inlet/outlet valves and the raw material remains in the first vessel on account of the filter. The valves are closed following
15 transfer of the solvent and before cooling is commenced.

On cooling, the extracted oil precipitates out of solution and begins to aggregate. Since the extracted oil is invariably significantly less dense than the solvent medium the extracted oil floats on the top of the solvent layer as a separate
20 immiscible/insoluble layer. The extracted oil can thus be easily separated by decanting. The solvent, which is almost entirely free of the oil, can then be returned to the first vessel for use in a further extraction cycle. This process can be repeated several times if desired. From a practical point of view, 10 cycles is the upper limit with 3 to 5 cycles being preferred on the basis of efficiency and time.

25

This manual procedure, though highly effective, was somewhat tedious to carry out and the whole process is preferably performed as a continuous operation as described above.

30 **Temperature difference between vessels (1) and (2)**

For maximum economic use of equipment designed to prepare extracts such as those of interest such as fixed or mineral oils, it is beneficial to operate vessels (1) and (2) at widely dissimilar temperatures. (The difference between these temperatures is commonly referred to as " ΔT "). The larger the " ΔT " the better the equipment will perform.

However, limits on " ΔT " are imposed by the design and fabrication of the equipment.

Upper limit of operating temperature of Vessel (1)

When iodotrifluoromethane is used, whether mixed with another solvent or not, a rise in the temperature of operation of Vessel (1) will automatically cause an increase in the pressure (vapour pressure) within the sealed system. Indeed, the highest operating temperature of vessel (1) must obviously never exceed, and must be less than, the "critical temperature" of the solvent (mixture) in use.

Also this highest operating temperature would be limited to a temperature less than that above which damage to the raw-material or the extract might occur.

Lower limit of operating temperature of Vessel (2)

The operating temperature of Vessel (2) must be as low as can be conveniently arranged. Sub-ambient and even refrigeration temperatures can be used.

The lower limit of operation of Vessel (2) will be determined by the characteristics of the solution (and its ability to dissolve solute). The solute must dissolve in the solvent as "poorly" as can be arranged and the "poverty" of this dissolution can be enhanced by lowering the temperature of operation of Vessel (2). The low limit is also governed by the viscosity of the resulting oil since at very low temperatures some oils may become difficult to handle.

The operation of the equipment is described for the purpose of illustration only as follows in relation to the extraction of an essential i.e. volatile oil: the substrate containing the essential oil is introduced into an extractor, having the shape of a flanged tube and furnished with removable end caps, each of which comprises a plate and a sheet of stainless steel mesh secured thereon to form a filter. The end caps or plates are also equipped with a port which is capable of closure and through which both gases and liquids can pass via the stainless steel filter mesh.

The extractor is closed and air is pumped out to a pressure of less than 40mbar. A source of supply of liquid iodotrifluoromethane is connected to the extractor and liquid solvent is allowed to pass to the extractor. The contents of the extractor are thus bathed in iodotrifluoromethane. The extractor is then sealed as the source of iodotrifluoromethane is disconnected. The extractor is then tumbled on its lateral axis for a period of time to ensure intimate contact between the solvent and the substance.

After the tumbling has stopped, the outlet is connected via alternative pipework to a small evaporator which has previously been evacuated to a pressure of 40mbar. The solution of oil in the iodotrifluoromethane solvent is allowed to pass intermittently from the extractor into the evaporator, to retain a level of liquid and gas filled headspace in the evaporator. The evaporator is then connected to the inlet of a compressor which is allowed to withdraw iodotrifluoromethane gas from the head space of the evaporator and to compress the gas (on its outlet side) to a pressure in excess of 5 bar.

A this pressure, and at room temperature, the gas is reliquefied and can either be recycled to the extractor to flush out residual oil or be reintroduced to the original reservoir of solvent for re-use on a further bath.

Inevitably, during this process the evaporator cools to very low temperatures and it is desirable to immerse it in a water bath furnished with an immersion heater and a

thermostat. The thermostat can be set to activate the immersion heater when the water temperature falls to for example 10°C and to switch off the heater whenever the temperature of the water exceeds for example 12°C. In this manner, the evaporator may be operated at about 10°C and the vapour pressure is 1 to 3 bar at the
5 compressor inlet.

The pressure contained the evaporator throughout this process is in the region of 30 psi. Once all the solution has passed from the extractor to the evaporator, and all the solvent from both the extractor and the evaporator has been evaporated, the vapour
10 pressure inside the evaporator begins to fall.

When this pressure had fallen to just above 0 psig an outlet on the bottom of the evaporator is opened so the oil solute (the extract) can run into a suitable receptacle. Weighing of the receptacle before and after the introduction of the oil reveals the
15 yield of fragrant oil.

Following removal of the oil, the compressor can be allowed to continue to suck residual solvent vapour from the extractor and from the substrate within it. By the time the pressure within the extractor has fallen to 100mbar over 99.9% of the
20 iodotrifluoromethane solvent will have been returned to the original reservoir.

To improve the recovery of solvent the extractor and the extracted substrate can be heated.

25 The present invention will now be illustrated by means of the following examples.

Example 1

At an ambient temperature of 20 degrees Celsius, 140 grams of peanut oil were
30 introduced into a PET bottle of capacity 2500 ml and designed to withstand 10 BarG. The bottle was fitted with an aerosol valve. This oil was dissolved in 780 grams of

iodotrifluoromethane which was introduced into the bottle, via the aerosol valve, from a bulk container.

The solution formed was crystal clear and pale yellow in colour. It formed a
5 completely homogeneous solution, a single phase.

HFC 134a was then introduced into the bottle via the aerosol valve from a similar bulk storage container, until the mixture separated into two distinct layers. The bottle was weighed to ascertain how much HFC 134a had been added. This proved to be
10 440 grams of HFC 134a. The upper layer of the two phase system was yellow and clear. The lower layer was clear and water white.

Warming this two phase mixture to 42 degrees Celsius with gentle agitation for a few seconds, caused it to become clear. It formed a single phase homogeneous solution.
15

Upon cooling, a two phase system re-formed, with the yellow layer lying on top of a clear water white layer.

The composition of the solvent in this case was 36.1% HFC 134a:63.9% ITFM w/w.
20

Example 2

At an ambient temperature of 20 degrees Celsius, 140 grams of peanut oil were introduced into a PET bottle similar to that of Example 1. On this occasion, 810
25 grams of iodotrifluoromethane were introduced into the bottle via the aerosol valve. A yellow, bright homogeneous solution was obtained.

On this occasion, 440 grams of HFC 134a were introduced into the bottle. The contents of the bottle remained as a single phase, slightly opalescent solution.
30

Cooling this solution to 4 degrees Celsius caused it to separate into a "two phase" system. The upper layer being yellow and the lower layer being clear and water white. Allowing this mixture to warm to room temperature (20 degrees Celsius) with gentle agitation, caused the two phase mixture to revert to its original state as a single
5 phase, homogeneous (if slightly opalescent) solution.

The composition of the solvent in this case was 35.3% HFC 134a:64.8% ITFM w/w.

Example 3

10

224 grams of finely ground sesame seeds were introduced into a 2500 ml capacity PET bottle fitted with an aerosol valve, at an ambient temperature of 20 degrees Celsius. 780 grams of iodotrifluoromethane was introduced to the bottle via the aerosol valve from a bulk container.

15

Shaking the bottle caused a distribution of the sesame seed paste. The bio-mass floated to the top as the specific gravity of the ITFM is close to 2.0.

To this mixture was added 480 grams of HFC 134a. Placing this mixture in the
20 fridge at 4 degrees Celsius caused agglomeration of the bio-mass. A single lump of solids was obtained which could not be easily broken up with shaking. This was assumed to be due to the precipitated oil and sesame seed bio-mass becoming re-mixed.

25 Allowing this mixture to warm to room temperature caused re-dissolution of the oil and the sesame seed bio-mass was then much easier to disperse in the liquid.

The liquid phase of this mixture was harvested by inverting the bottle, via a filter attached to the aerosol valve, into a second PET container. A clear homogeneous
30 liquid was obtained.

Refrigeration of this liquid caused it to separate into two layers. Both layers could be harvested separately (by inverting the bottle) and the lower layer was found to contain mostly solvent whilst the upper layer comprised mostly oil (with a little solvent dissolved in it).

5

The composition of the solvent in this case was 38% HFC 134a:62% ITFM w/w.

Example 4

10 20 grams of peanut butter (Sun Pat) were introduced into a 210 ml capacity PET bottle fitted with an aerosol valve and filter. 195 grams of ITFM were added. The mixture formed a cream coloured, even dispersion. 101 grams of HFC 134a were then added and the mixture shaken. The solution was filtered into a new PET bottle. 274 grams of solution were recovered.

15

To this solution was added a further 7 grams of HFC 134a. It remained as a single phase.

A further 5 grams of HFC 134a were added. The mixture was now refrigerated and
20 two distinct layers formed. The lower layer of this solution was recovered and added to a further 141 grams of peanut butter at 20 degrees Celsius. A milky even dispersion of creamy coloured peanut bio-mass was formed. This mixture was again filtered back into the bottle in which the solution had originally been filtered and the combined filtrates were again refrigerated.

25

Refrigeration of this solution caused a great deal of oil to precipitate out of solution and a thick layer of yellow oil formed on the surface. This oily material was easily recovered by inverting the bottle following the removal of the lower (largely solvent) layer.

30

The composition of the solvent in this mixture was 37% HFC 134A:63% ITFM w/w.

Example 5

28 grams of ground roasted cocoa beans were placed into a 210 ml capacity PET
5 bottle and an aerosol valve with filter was attached. 189 grams of ITFM were added
and 106 grams of HFC 134a.

The mixture was filtered into a second bottle and refrigerated to minus 10 degrees
Celsius. White, solid, cocoa butter was seen to rise to the surface. Re-warming of
10 this bottle to room temperature caused the cocoa butter to melt, re-dissolve and
become homogeneously distributed throughout the liquid phase.

The composition of the solvent in this mixture was 36% HFC 134a:64% ITFM w/w.

15 The present invention thus addresses many of the disadvantages discussed above and
provides a means of obtaining fixed oils and mineral oils in good yields in a form
approaching 100% purity.

CLAIMS

1. A method of extracting oil from an oil-bearing substrate comprising:
 - (a) contacting the substrate with a solvent comprising and, optionally, one
5 or more co-solvents to form a solution of the oil in the solvent;
 - (b) separating the solution from the substrate; and
 - (c) removing the solvent from the solution to provide the desired oil.
- 10 2. A method as claimed in claim 1 further comprising contacting the solvent with the substrate in a first vessel and separating the resulting solution from the substrate by transferring the solution to a second vessel while retaining the extracted substrate in the first vessel.
- 15 3. A method as claimed in claim 2 wherein the first and second vessels are each sealable and each include an openable and closable valve, the method further comprising the steps of:
 - (i) connecting the vessels together to provide a flow path between the
vessels via said valves; and
 - (ii) causing the solution to flow from the first vessel to the second vessel.
20
4. A method as claimed in claim 2 or 3 further comprising the step of applying heat to heat the solvent in the first vessel.
- 25 5. A method as claimed in any of claims 2 to 4 further comprising the step of cooling the solution in the second vessel.
- 30 6. A method of extracting oil from an oil-bearing substrate comprising:
 - (a) providing an apparatus comprising first and second sealable vessels, the first vessel including means for retaining said substrate in the vessel, each vessel having an inlet and an outlet and being so connected as to provide a fluid flow circuit only in the direction from the outlet of the first vessel to the

inlet of the second vessel and from the outlet of the second vessel to the inlet of the first vessel;

(ii) charging the oil bearing substrate into the first vessel;

5 (iii) charging the apparatus with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents so that the solvent contacts the substrate and forms a solution of the oil in the solvent;

(iv) causing said solution to flow in said fluid flow circuit from the first vessel to the second vessel; and

10 (v) separating the solvent from the oil in the second vessel and recovering the oil.

7. A method as claimed in claim 6 further comprising the step of applying heat to the solvent in the first vessel, or adjacent the inlet of the first vessel.

15 8. A method as claimed in claim 6 or 7 further comprising the step of cooling the contents of the second vessel.

9. A method as claimed in any of claims 6 to 8 further comprising recovering the separated solvent for use in further extractions.

20

10. A method as claimed in any preceding claim wherein the optional co-solvent is selected from HFC 134a and HFC 4310.

25 11. An apparatus for the extraction of oil from an oil bearing substrate comprising first and second vessels, connecting means providing fluid communication between the vessels, at least one closable valve operable to prevent fluid communication between the vessels, the first vessel being adapted to receive the oil bearing substrate and including means for retaining the substrate in the first vessel, and, a solvent provided in the first vessel
30 comprising iodotrifluoromethane and, optionally at least one co-solvent.

which solvent may be transferred between the first and second vessels via the or each closable valve.

- 5 12. An apparatus as claimed in claim 11 wherein each vessel comprises an inlet and an outlet, the outlet of the first vessel is connected by first connecting means to the inlet of the second vessel, the outlet of the second vessel is connected by second connecting means to the inlet of the first vessel, the first and second connecting means include at least one said closable valve, and each closable valve is a one-way valve permitting fluid flow in one direction only, the valves being arranged to provide a fluid flow circuit such that the solvent may flow around the circuit in one direction only.
- 10
13. An apparatus as claimed in claim 12 wherein one closable one-way valve is provided at each respective inlet and each respective outlet of the first and second vessels.
- 15
14. An apparatus as claimed in claim 12 or 13 including heating means for heating the solvent in the first vessel or adjacent to the inlet of the first vessel.
- 20 15. An apparatus as claimed in any of claims 12 to 14 including cooling means for cooling the contents of the second vessel.
16. An apparatus as claimed in any of claims 11 to 15 further comprising a reservoir of solvent operatively connectable to the fluid flow circuit.
- 25
17. Apparatus as claimed in any of claims 11 to 16 further comprising means for withdrawing, from the second vessel or from the connecting means adjacent the second vessel, oil which has separated from the solvent.
- 30 18. A method of extracting oil from an oil bearing substrate comprising the steps of:

- (i) contacting the substrate with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents thereby to dissolve the oil in the solvent; and
- (ii) causing the oil to separate from the solvent to form immiscible liquid layers of oil and solvent.
- 5
19. A method as claimed in claim 18 wherein step (ii) involves cooling the solution of oil in the solvent.
- 10 20. A method as claimed in claim 18 or 19 wherein step (i) includes heating the solvent.
21. A method of extracting oil from an oil-bearing substrate comprising the steps of:
- 15 (i) contacting the substrate with a solvent comprising iodotrifluoromethane and, optionally, one or more co-solvents, thereby to dissolve the oil in the solvent; and
- (ii) allowing the solvent to evaporate at ambient or sub-ambient temperatures.
- 20
22. A method as claimed in claim 21 further comprising recovering the evaporated solvent and compressing the solvent to re-liquify it.
23. Use of iodotrifluoromethane for the extraction of oil from an oil-bearing substrate.
- 25
24. Use of a solvent comprising iodotrifluoromethane and at least one co-solvent for the extraction of oil from an oil-bearing substrate.
- 30 25. An oil obtainable by, or when obtained by, the method of any of claims 1 to 10 or 18 to 22.

26. A vegetable oil for use in foodstuffs obtainable by, or when obtained by, the method of any of claims 1 to 10 or 18 to 22 and containing substantially no residue of solvent, especially iodotrifluoromethane.

5

